



Viral vectors - Overcoming process challenges to meet the clinical demands

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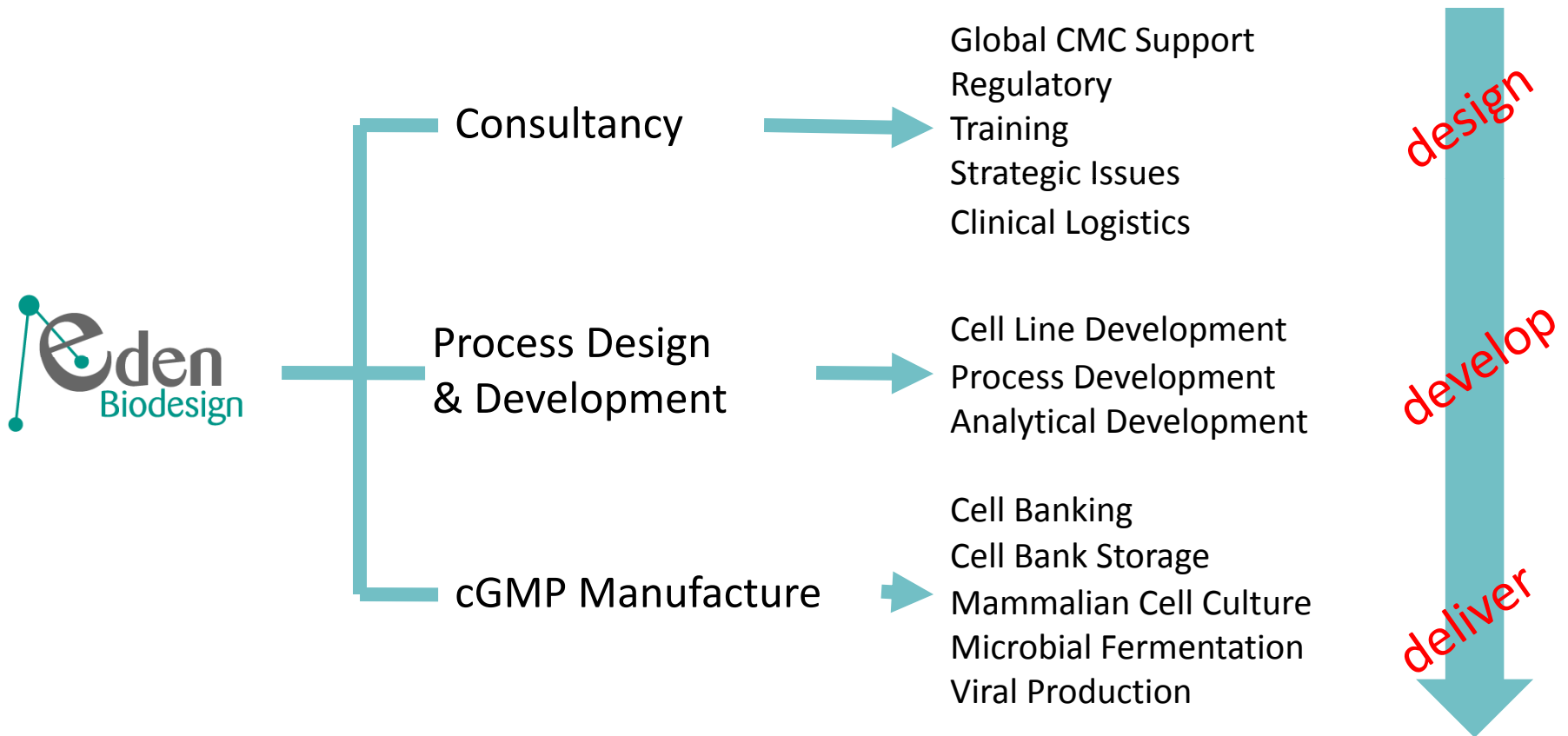
Questions

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An unusual breadth and depth of services supported by considerable drug development experience and expertise



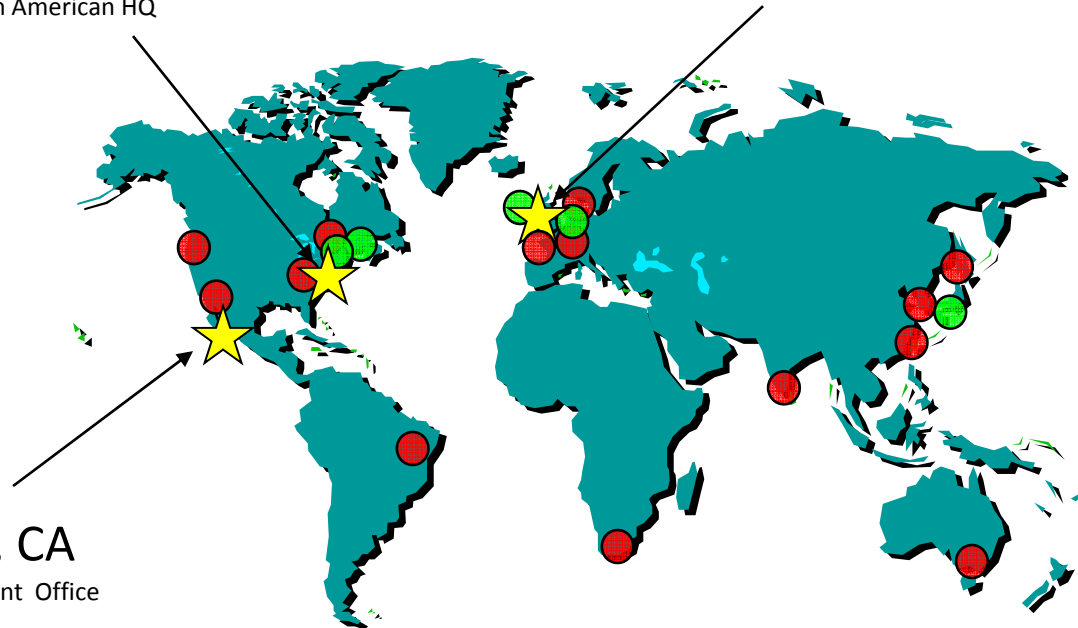
Eden Biodesign Maintains a Globally Integrated Biopharmaceutical Network



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Clients on
six of seven
continents

● *Client Assignments*

★ *Eden Presence*

● *Strategic Partners*

DESIGN • DEVELOP • DELIVER

Presentation Overview



- ❑ Challenges of viral production
- ❑ Historical processes
- ❑ Targets for success
- ❑ Upstream development requirements
- ❑ Case study
 - USP strategy
 - DSP & process sighting
- ❑ Scale up
- ❑ Conclusions

The Challenges.....



- ❑ Recent resurgence in live viral products
 - Gene therapy
 - Vaccines
- ❑ Typical Tox & Phase I = E+15 VP (E+13/14 IU)
- ❑ Typically research based processes

“Historical” Processes



❑ Adherent based systems

- CPE as harvest indicator
- Small scale

❑ CsCl purification

- Process is an impurity
- High Cap ex outlay
- Scalable? Volume limited

❑ Inappropriate analytics

- Activity indicating plaque assay – time consuming etc
- Limited information on product quality



The Bioprocessing Targets...



- ❑ Suspension USP processes
 - Scalable
 - Appropriate for multiple backgrounds

- ❑ Platform DSP processes
 - Scalable
 - Appropriate impurity profiles

- ❑ Rapid development strategies
 - MOI/POI/POH studies
 - Process sighting
 - MVSS feasibility

- ❑ Rapid, platform & appropriate analytics
- ❑ Reduced C of G's

Upstream Development



- Generation of suspension cell lines
 - Serum weaning
 - Media development
 - Kinetics & aggregation state

- Cell banking investigation (Development based)
 - DMSO hold
 - Cell bank size
 - QC cell bank revival specifications
 - Process sighting



Case Study



Case Study



- ❑ Ad5 serotype containing transgene of clinical importance
- ❑ Suspension adapted cell line
- ❑ Rapid USP development strategy
 - Small scale and comparative
 - Appropriate analytics
- ❑ Platform DSP
 - Process sighting and scale up

Case Study - Appropriate Analytics



- Rapid development strategy
 - Rapid Titre (Hexon staining)

- Process sighting & exemplification (Pilot scale)
 - Rapid Titre
 - CIM[®] QA HPLC (Whitfield RJ *et al.*, *J Chromatography A*. 2009)
 - HCDNA
 - HCP
 - Residual Benzoylase
 - *Transgene (product specific)*
 - *Activity (product specific)*



Case Study - Typical Analysis



Step	Sample	Volume (mL)	Analysis
Harvest	Bioreactor sample	1988	RT
Cell disruption	Postlysis	1000	AEX, DNA ¹
Clarification 1	Clarified supernatant	938	RT, SDS, AEX, DNA ¹
Nuclease reduction	Post Nuclease	938	RT, SDS, AEX, DNA¹
UF/DF	Permeate	1788	SDS, AEX, DNA¹
	Retentate	230	RT, SDS, AEX, DNA¹
Clarification 2	Post 0.55 µm filtration	192	SDS, AEX, DNA
Anion exchange	Peak 1 (also GS load)	14	RT, SDS, AEX, DNA¹
	Peak 2	17.5	SDS, AEX
Group separations	Main peak eluate	27	RT, SDS, AEX, DNA¹

RT = Rapid titre

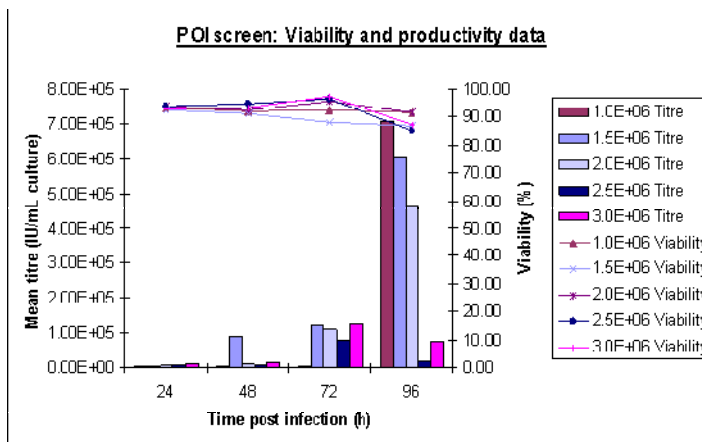
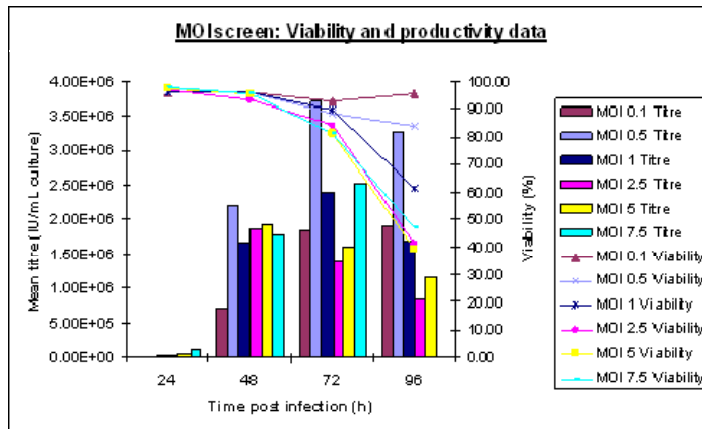
SDS = Reduced SDS-PAGE

AEX = Anion exchange HPLC

DNA¹ = Analysis via Picogreen assay

DNA² = Analysis via qPCR

Case Study - USP Approach



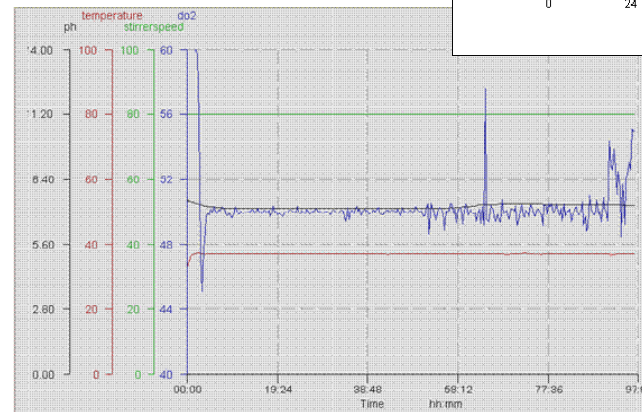
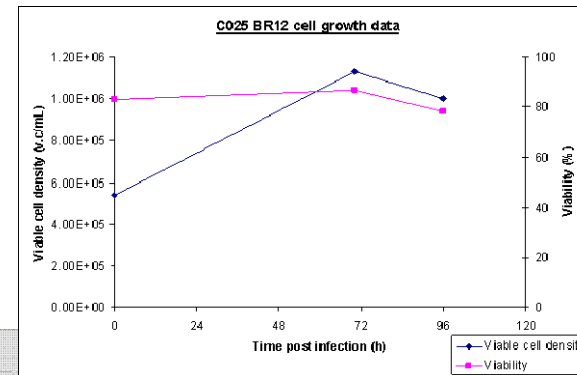
- Rapid development strategy
- 50mL shake flasks scale
- MOI, POI & POH
 - Primary indicator - process viability
 - Process titre determined
- Lower than expected MOI's
 - Smaller MVSS
- Process titre variance
 - 96 h duration confirmed

Case Study - Bioreactor



□ 2.5 L stirred tank format

- Process sighting
- Baseline process controls
- Developed critical controls
 - MOI = 0.5
 - POI = $5.0E+05$ vc/mL
 - POH = 96 h



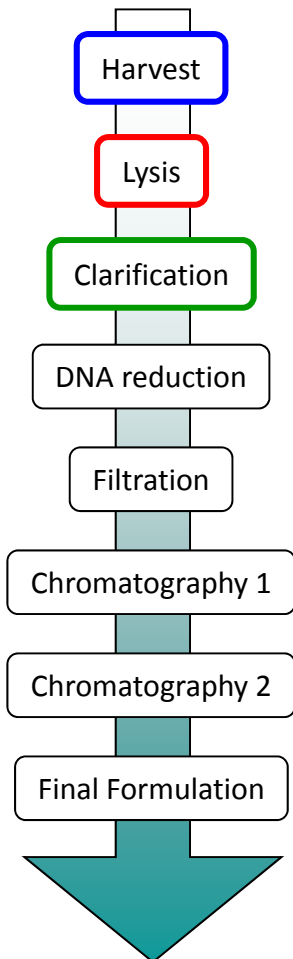
□ Harvest titre = $4.5 E+10$ IU (2L)

Case Study – DSP Approach



- Platform CIM[®] QA monolith process
 - Process sighting
 - Identify process changes if required
 - Decisions based on impurity profile & scalable unit activities

Case Study - DSP



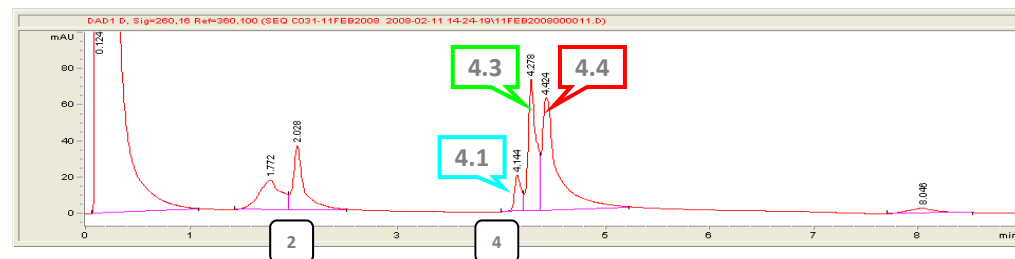
□ Harvest = Batch centrifugation

➤ TFF under development

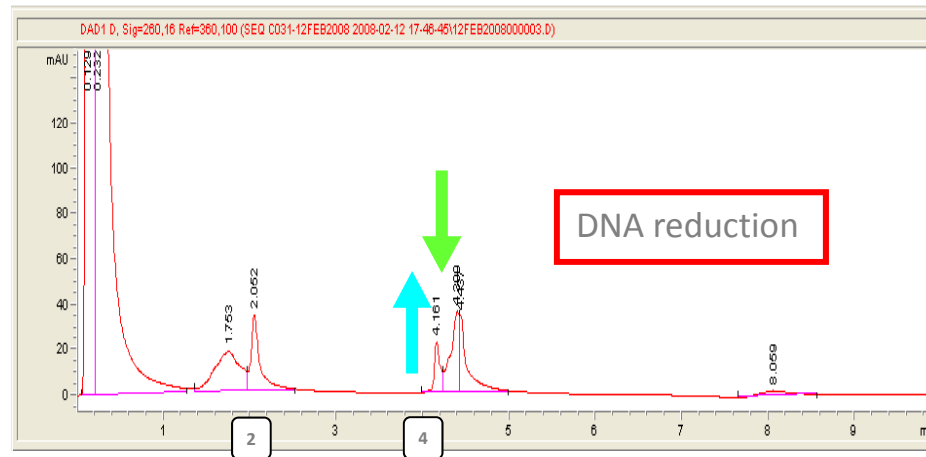
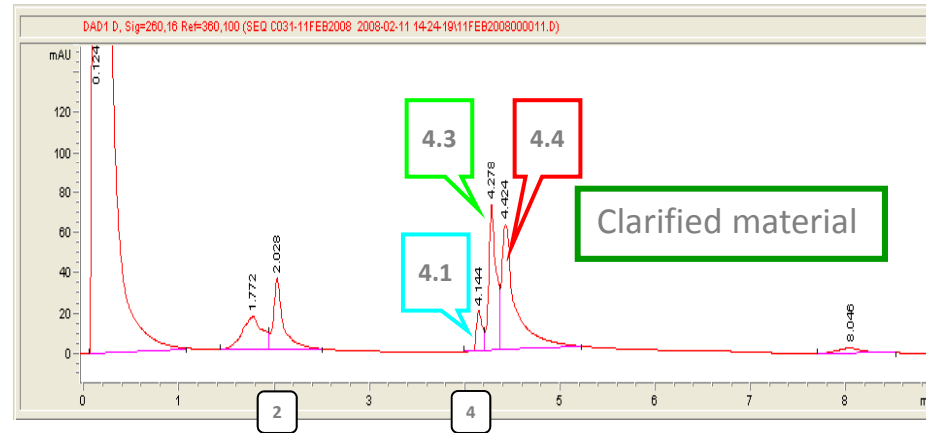
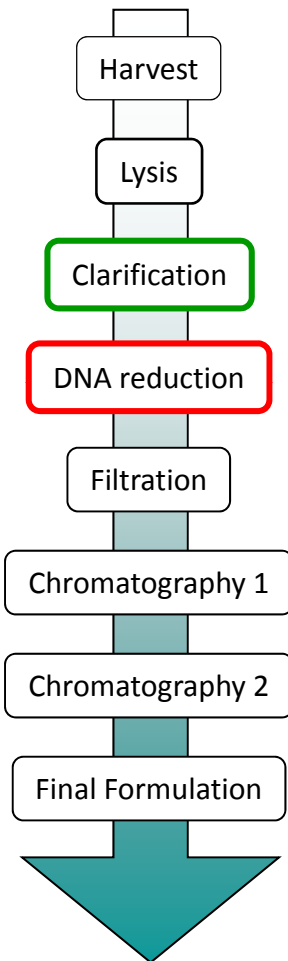
➤ Natural -80C hold point if required

□ Lysis = Lysis buffer (50% volume reduction)

□ Clarification = Batch centrifugation

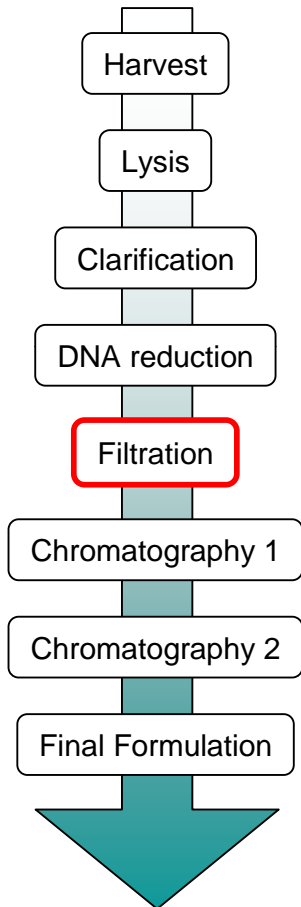


Case Study - DSP

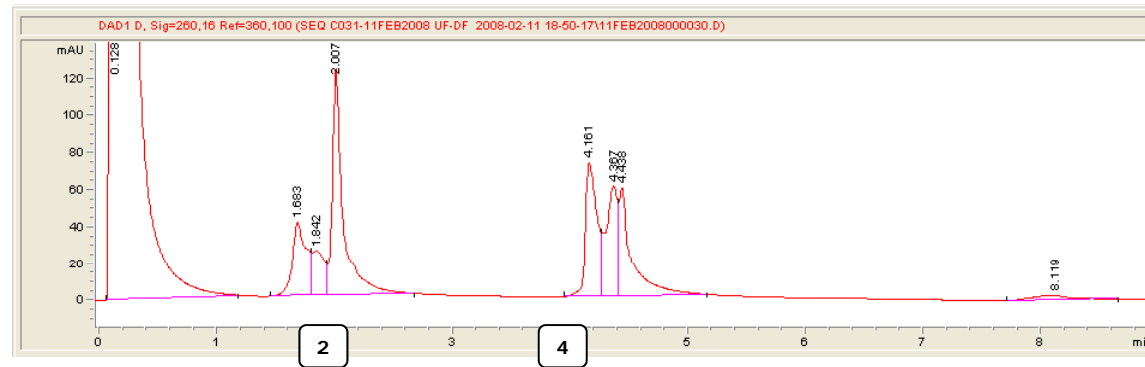


□ HCDNA = Below levels of detection

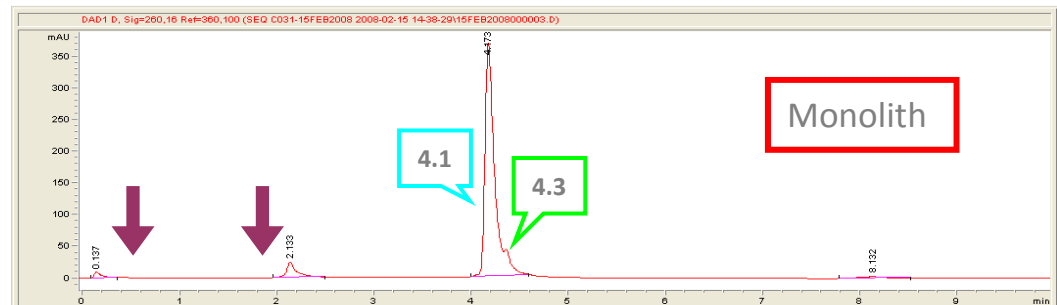
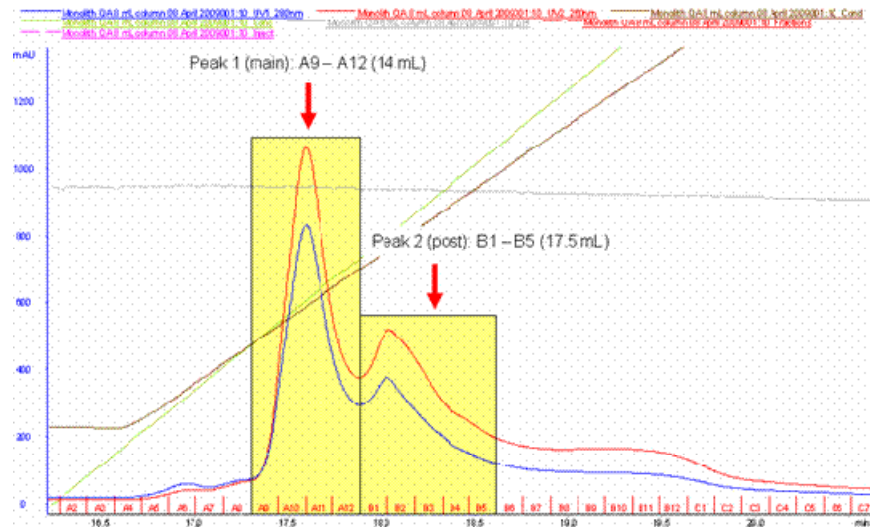
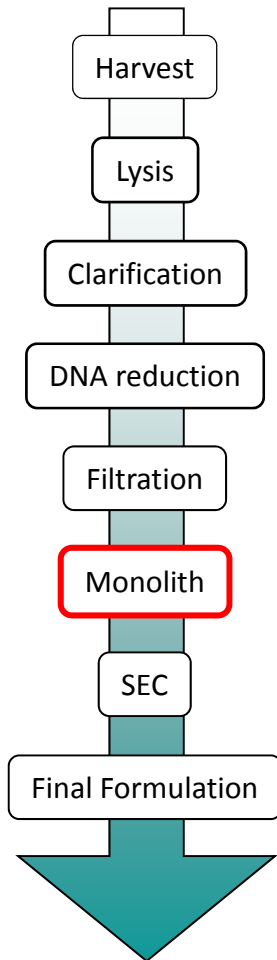
Case Study - DSP



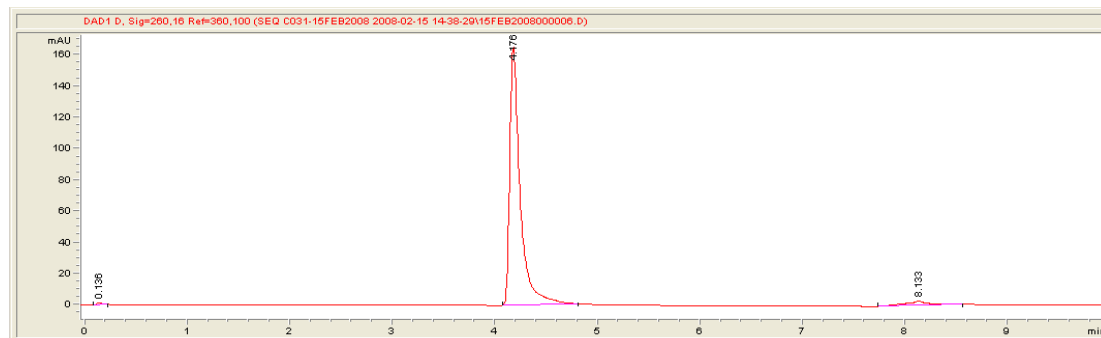
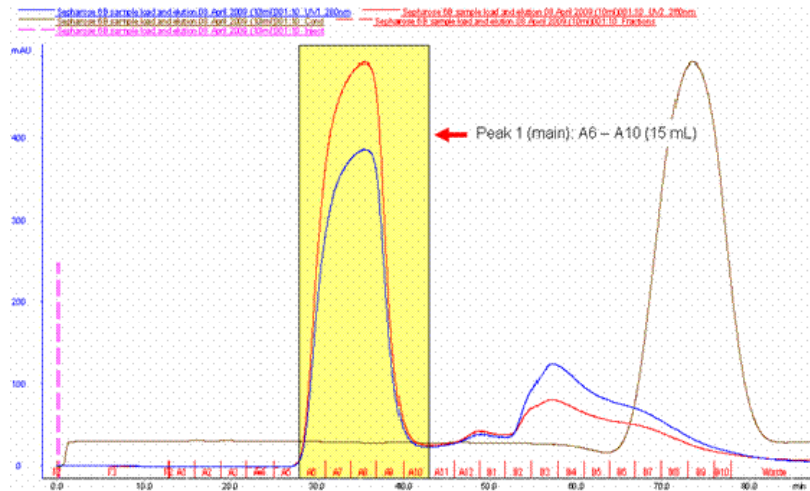
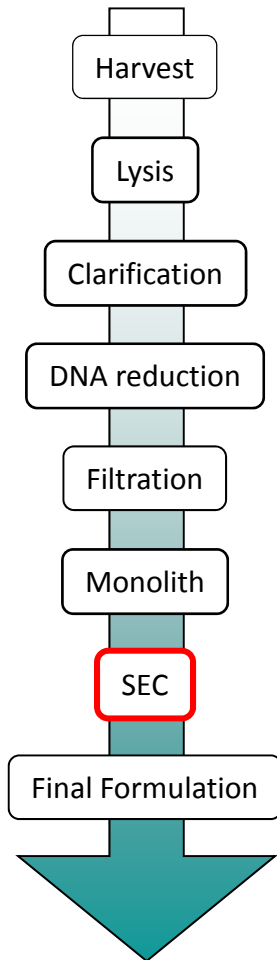
- UF/DF exchange into appropriate AEX buffer
- Reduce residual benzonase & 5X vol reduction



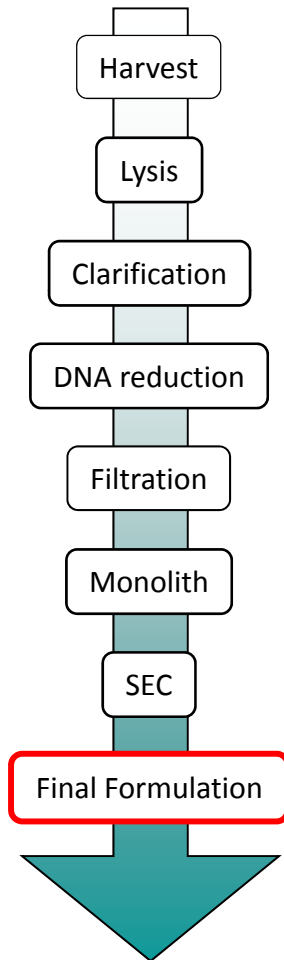
CIM[®] QA Monolith column chromatography



Size Exclusion Chromatography

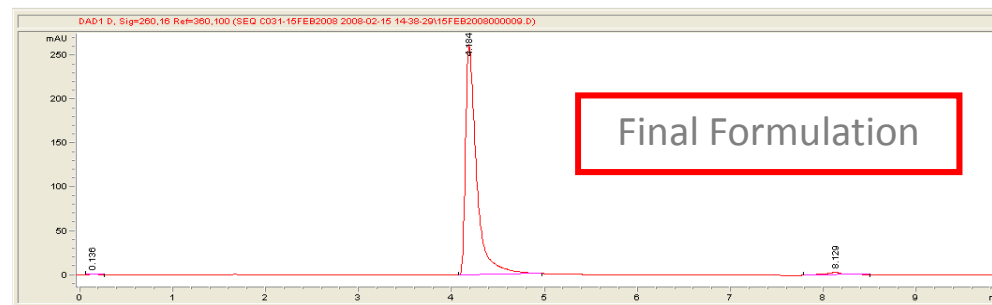


Final Formulation

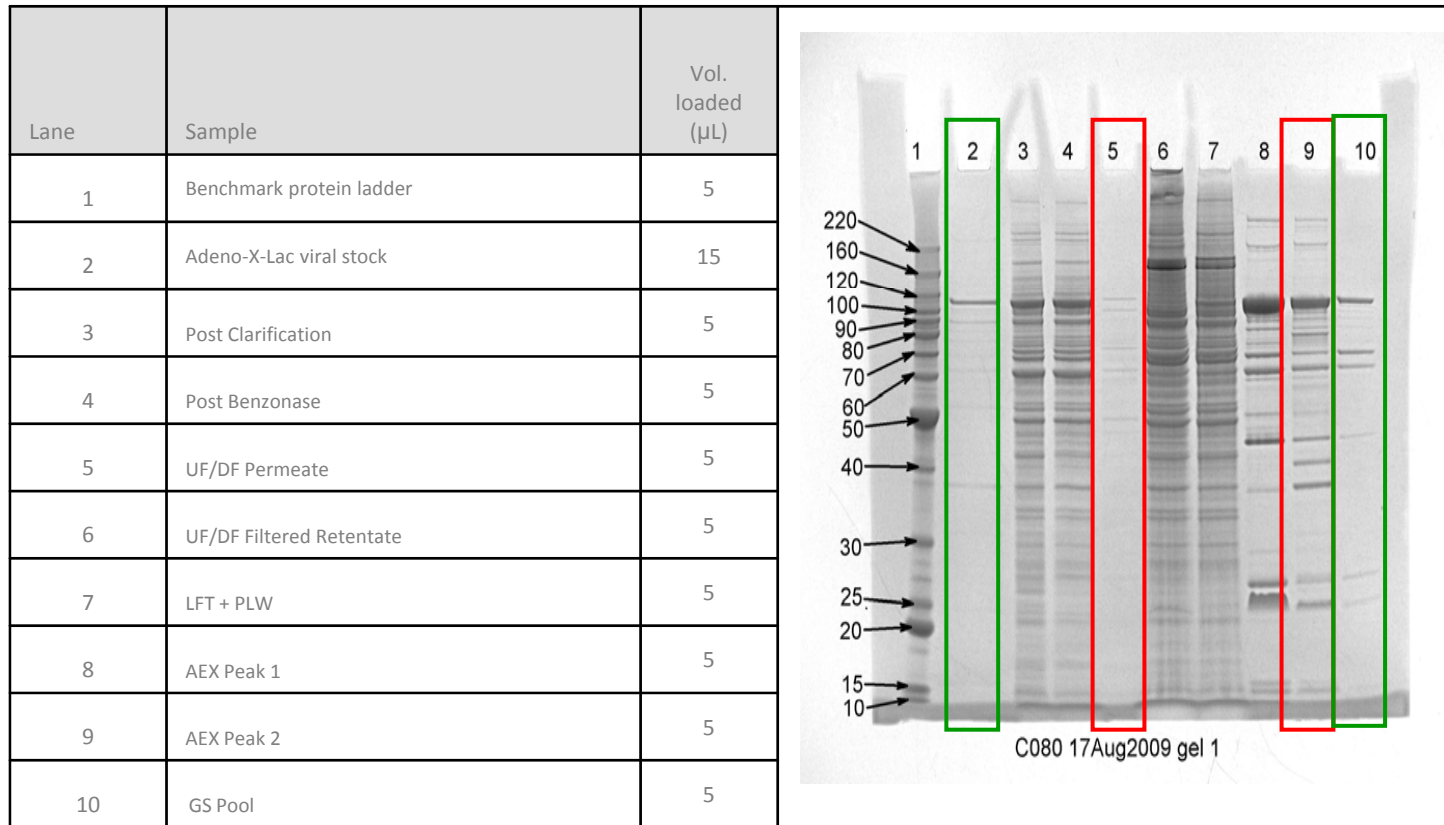


□ UF/DF into final buffer formulation

- Client supplied formulation
- Appropriate concentration (Concentration/reduction)
- Appropriate for route of administration



Case Study – Product Integrity



Reducing SDS-PAGE

Case Study – Process Sighting



- ❑ Harvest titre = 4.5 E+10 IU (2L)
 - Assay interference with spent media
- ❑ Final product 4.56E+11 IU (2L)
- ❑ Final product 8.02E+12 VP (2L)
- ❑ VP:IU ratio ~17.5:1 (Typically 20:1)
- ❑ Good impurity profile
 - Residual HCDNA, HCP, Benzonase – not detectable

Scale up



- Appropriate for variant cell backgrounds
 - Developed process controls applied
 - Culture kinetic remain similar to 2L scale bioreactor

- DSP appropriate for scale up
 - Differences in AEX profile at scale
 - Impurity profile

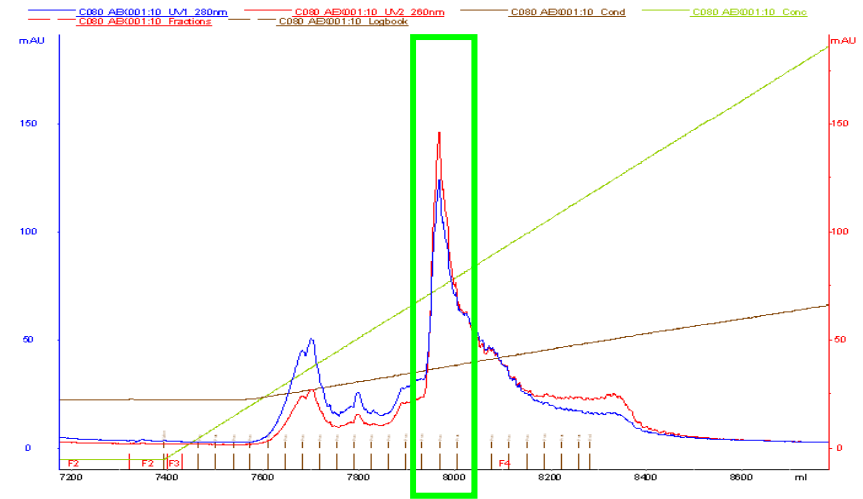
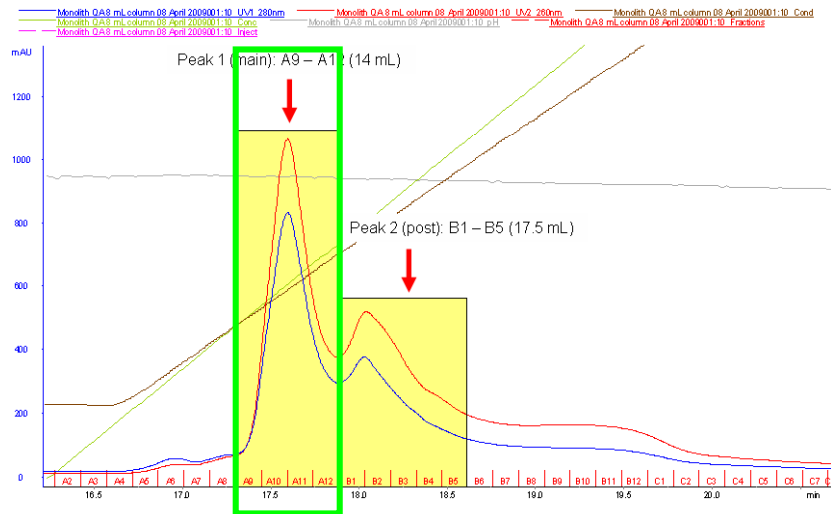
2.0 – 20L Scale up



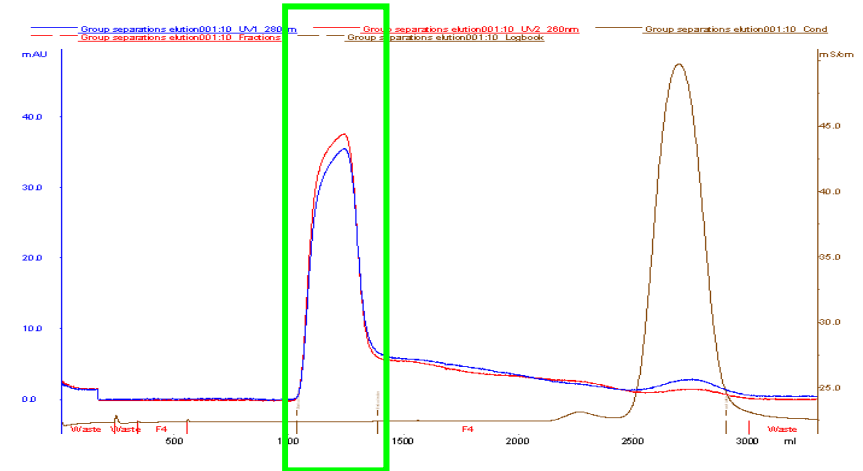
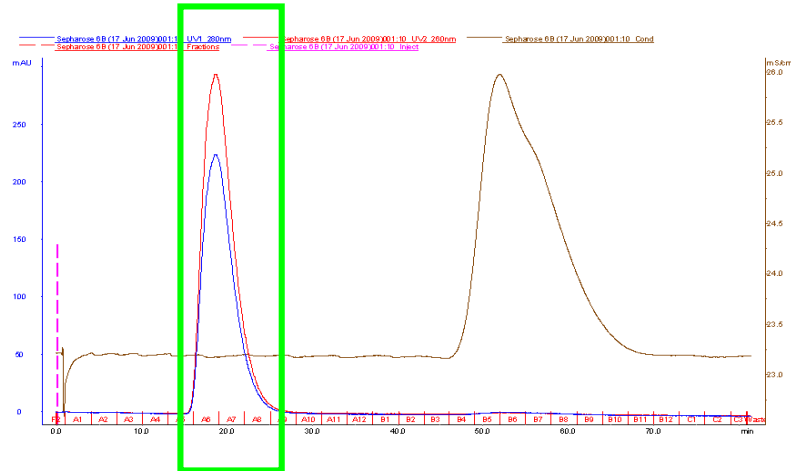
2L (STR & DSP)

20L (STR & DSP)

CIM® QA Monolith



SEC (Group sep)



Conclusions



- ❑ Suspension based process supports:
 - Rapid, comparative development strategy
 - Scaled, STR based batch production
- ❑ DSP process tolerates challenge from various USP backgrounds (Ad5 serotype) and scale up issues
 - Robust analytics demonstrate identical impurity profiles as 2 & 20L scale
- ❑ Platform analytics support both rapid development activities and clinical batches
- ❑ Delivery of $\sim 5.0E+15$ VP ($\sim 2.4E+14$ IU) achievable
 - Reproducible impurity profile

Acknowledgments



□ Eden Biodesign:

- Jennifer Halsall (USP Virus Team Leader)
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- Phil Ball (Technical Director, US)

□ Invitrogen

- Jonathan Dempsey
- Louisa Paterson

□ BIA Separations:

- Miloš Barut
- Aleš Štrancar



Questions

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Thank You.



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